

## The Performance Analysis of a Venturimeter Flow Rig

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**Abstract:** This paper presents the performance analysis of a Venturimeter flow rig; designed and manufactured for use in the Mechanical Engineering Laboratory of the Akwa Ibom State University (AKSU), Ikot Akpaden, Nigeria. The project provides a portable flow measurement apparatus for flow measurement in the laboratory. The students will use this apparatus during their fluid mechanics practical, to determine the discharge of a flowing liquid through the meter, hence the measurement of flow rate across the Venturimeter. The idea will be essential to flow discharge measurement in petroleum pipeline, irrigation facilities, automotive industry, wastewater collection systems and treatment plants. The rig consists essentially of measuring tank reservoirs, the Venturimeter, sump tank, an electric motor, cable, plug, valves, Polyvinyl Chloride (PVC) piping connections and a U-tube manometer. The design and construction were done with strict compliance to international standards to provide a high precision target for the measurement of flow rate; the length of the divergent cone of the Venturimeter is three (3) times that of convergent cone. The ratio of the diameter at throat to that of the pipe was  $\frac{1}{2}$ . The manometer was used to measure pressures in the pipe, expressed in terms of head of water in metres. The Bernoulli's equation and the continuity equation were applied for the flow analysis. The values generated from the Venturimeter were validated against the standard Khurmi discharge values and were in good agreement as both plots shows similar trends; because, by increasing the value of the pressure head, there was a corresponding increase in discharge, hence confirming the efficacy of the Bernoulli's principles and continuity equation in the analysis of flow discharge through Venturimeter. This project is produced at a reduced cost since the materials used were sourced locally. The manufacturing cost will further reduce significantly if the Venturimeter flow rig is mass produced.

**Keywords:** Venturimeter, Pressure drop, Head, Flow Measurement, Rig and Laboratory.

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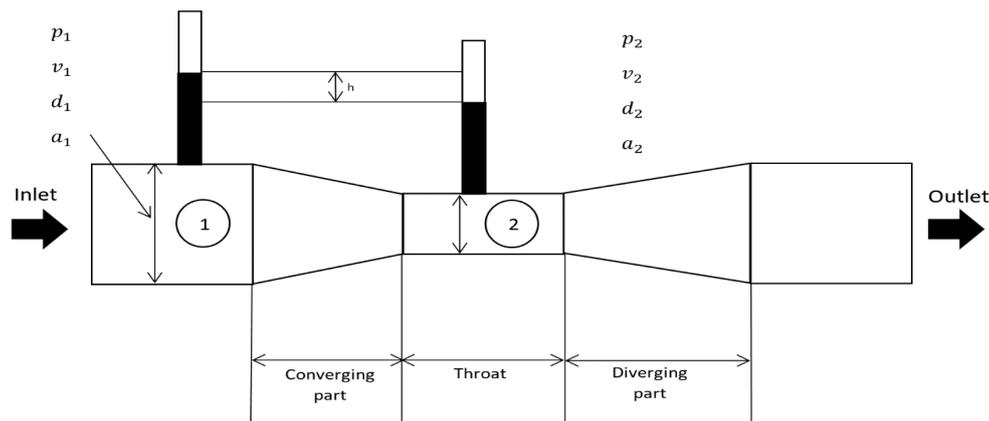
Date of Submission: 13-05-2020

Date of Acceptance: 26-05-2020

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### I. INTRODUCTION

A Venturimeter is a device used for measuring the rate of flow of a fluid flowing through a pipe. It is also an apparatus for finding out the discharge of a liquid flowing in a pipe. It consist of three main parts; convergent cone, throat and divergent cone. The convergent cone is a short pipe which converges from section 1 to a small diameter and it is known as the inlet of the Venturimeter. Divergent cone is the long pipe which diverges from the throat to a large diameter while the throat is the small portion of the circular pipe at which the convergent cone converges and the divergent cone diverges respectively as shown in Figure 1.1. It is vital to note that the short converging part of the Venturi is where the fluid gets converges, the throat section lies in between the converging and diverging part of the venture. The cross section of the throat is much less than the cross section of the converging and diverging section. When the fluid enters the throat its velocity increases and the pressure decrease. The length of the divergent cone is about three (3) to four (4) times than that of the convergent cone.



**Figure 1.1: Cross section of Venturimeter showing variations in pressure (p), velocity (v), diameter (d) and area (a) (Effiong, W. C. 2017)**

A Venturimeter uses a converging section of pipe to give an increase in the flow velocity and a corresponding pressure drop from which the flow rate can be deduced. They have been in common use for many years, especially in the water supply industry (Harris, 2011).

This flow measurement apparatus is used in the practical application of Bernoulli's theorem to the measurement of fluids flowing in pipes under pressure. Hence, the working of Venturimeter is based on the principle of Bernoulli's and continuity equations. The Bernoulli's principle states that in a steady, ideal flow of an incompressible fluid, the total energy at any point of the fluid is constant. The total energy consists of pressure energy, kinetic energy and potential energy.

A Venturimeter fit into the same class of flow measuring instruments known as Head meters such as the orifice meter. The short converging part is a tapered portion, whose radius decreases as we move forward. The middle portion of the Venturi is known as the throat. At the throat, the velocity of the fluid increases and pressure decreases. It possesses the least cross section area. After the throat, is the diverging part, where the fluid diverges.

The upstream section is a contracting portion with included an angle of from 19 to 23 degrees while the downstream section is a portion of a cone diverging with include an angle of 5 to 15 degrees. The throat can also be described as the junction of the two reduced sections of the Venturi. There are two pressure taps located in the Venturi.

The versatile application of Venturimeter in industries and medical practices required the practical introduction of the apparatus for students studying fluid mechanics; for flow measurement experiments. Noting that a majority of engineering students learns best when exposed to hands-on exercises and activities; hence, the analysis of this manufactured flow measurement equipment using Venturimeter for Mechanical Engineering Laboratory in Akwa Ibom State University, Nigeria.

The aim of this work is to analysis the discharge performance of the manufactured Venturimeter flow rig in use at Mechanical Engineering Laboratory AKSU shown as Figure 1.2 by applying the Bernoulli's and continuity equation respectively, and validating the results against a known standard Khurmi (2006) experiment for accuracy. Figure 1.2 shows the manufactured Venturimeter flow rig being integrated alongside other fluid mechanics equipment in the fluid mechanics laboratory in AKSU.



**Figure 1.2: Shows the manufactured Venturimeter flow rig being integrated alongside other fluid mechanics equipment in the fluid mechanics laboratory in AKSU, Nigeria**

## II. A REVIEW OF SOME WORK USING VENTURIMETER

In fluid dynamics, Bernoulli's principle states that an increase in the speed of a fluid occurs simultaneously with a decrease in pressure or a decrease in the fluid's potential energy (Clancy, 1975; Batchelor, 1967). Bernoulli's principle can also be derived directly from Isaac Newton's Second Law of Motion. If a small volume of fluid is flowing horizontally from a region of high pressure to a region of low pressure, then there is more pressure behind than in front. This gives a net force on the volume, accelerating it along the streamline (Babinsky, 2003; Weltner and Ingelman-Sundberg, 2009). Fluid particles are subject only to pressure and their own weight. If a fluid is flowing horizontally and along a section of a streamline, where the speed increases, it can only be because the fluid on that section has moved from a region of higher pressure to a region of lower pressure; and if its speed decreases, it can only be because it has moved from a region of lower pressure to a region of higher pressure. Consequently, within a fluid flowing horizontally, the highest speed occurs where the pressure is lowest, and the lowest speed occurs where the pressure is highest (Resnick and Halliday, 1960).

The use of this instrument in laboratories to monitor flow rate and hence model or simulate real life flow scenarios is very essential. This is evident in various works done by different authors on the need of applying the principle of Venturimeter for flow measurement and analysis in petroleum pipeline, irrigation facilities, automotive industry, wastewater collection systems and treatment plants, among others. Hasan E. (2010) undertook a research on the use of Venturimeter to measure flow rate of multiphase flows, where two or even three fluids flow simultaneously in a pipe. These types of flow are becoming increasingly important in industry. The new separated flow model according to Hasan is based on the measurement of the gas volume fraction at the inlet and the throat of the Venturi meter rather than relying on prior knowledge of the mass flow quality. According to Prasanna M. A *et al.* (2016), the analysis of flow through Venturimeter has demonstrated the capability of using Computational Fluid Dynamics (CFD) methodology for predicting accurately the values of the coefficient of discharge ( $C_d$ ), expansibility factor or expansion factor ( $\epsilon$ ) and permanent pressure loss coefficient (CPL) over a wide range of operating conditions. CFD methodology also has been used to analyze the effect of various parameters like surface roughness, convergent and divergent angle as well as turbulent intensity of the incoming flow on the expansibility factor. It has been demonstrated that the validated CFD methodology can be used to predict the performance parameters of a classical Venturimeter even under conditions not covered by ISO 5167-1 standards. Ameresh H. (2017) employed the finite element analysis (FEA) software ANSYS to calculate the mass flow rate values for Venturimeters by varying inlet diameter of these venturimeters. With wet gas metering becoming an increasingly important problem to the oil and gas

industry, the Venturimeter is a preferred piece of equipment for the metering of the unprocessed wet natural gas production flows. In view of the above, Musbah, A. and Lucas, G. (2012) carried out a study on the use of an advanced Conductance Venturimeter which is capable of measuring the gas volume fractions at the inlet and the throat of the Venturi to study the annular flow using a Venturi with conductance sensors. This model is based on the measurement of the gas volume fractions at the inlet and the throat of the Venturimeter using a conductance technique. Amaresh, K. D (2018) apply FLUENT software for the numerical analysis of different Venturimeter models to describe the performance parameters such as Velocity, Pressure and Flow rate. Since pipe carrying sediment laden flow or slurry-water mixture is a common feature in few industries pipeline flow, Kala A. *et al.* (2015) undertook an experimental research on the discharge characteristics of Venturimeter for sediment laden flow to show that the coefficient of discharge of flow varies with Reynolds number, sediment concentration and the size of sediment using three different sizes of sediments. This review shows the vital need of Venturimeter in flow measurement and control.

### III. METHODOLOGY

The methodology uses Bernoulli's theorem and Continuity equation in the analysis of the Venturimeter. The design principle of the Venturimeter is based on the theory of discharge of a liquid flowing in a pipe. During the flow of liquid through a pipe, there is an effect known as the Venturi effect. This effect is the reduction in fluid pressure that results when a fluid flows through a constricted section of the pipe. The fluid velocity must increase through the constriction to satisfy the equation of continuity, while its pressure must decrease due to conservation of energy: the gain in kinetic energy is balanced by a drop in pressure or a pressure gradient force. An equation for the drop in pressure due to Venturi effect is governed by Bernoulli's and continuity equations.

#### 3.1 Discharges through a Venturimeter

In this study, the performance characteristics of a Venturimeter are determined. Applying Bernoulli's theorem and Continuity equation; and according to Khurmi (2006) to a Venturimeter through which some liquid is flowing as shown in Figure 3.1 and for completeness,

Let

$p_1$  = Pressure at section 1

$v_1$  = Velocity of water at section 1

$Z_1$  = Datum head at section 1

$a_1$  = Area of the Venturimeter at section 1

$p_2, v_2, Z_2, a_2$  = Corresponding values at section 2

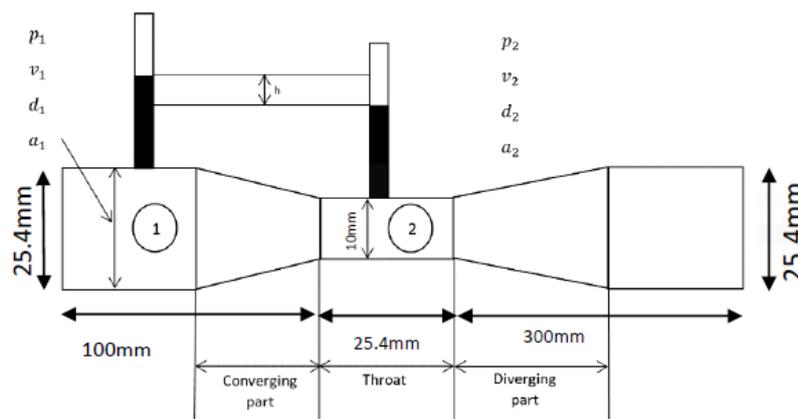


Figure 3.1: Venturimeter with dimensions as designed for the analysis (Effiong, W. C. 2017)

Applying Bernoulli's equation at section 1 and 2, we have that,

$$Z_1 + \frac{v_1^2}{2g} + \frac{p_1}{w} = Z_2 + \frac{v_2^2}{2g} + \frac{p_2}{w} \quad 3.1$$

Applying the Continuity equation at section 1 and 2, since the discharge is continuous, then,

$$v_1^2 = \frac{a_2^2 v_2^2}{a_1^2} \quad 3.2$$

Noting that the pipe is horizontal, then the difference between the pressure heads at sections 1 and 2 represents the Venturi head, denoted as  $h$ , hence the relationship between the velocity and the Venturi head is given as,

$$v_2 = \sqrt{2gh} \left( \frac{a_1^2}{a_1^2 - a_2^2} \right) \tag{3.3}$$

Having been acquainted with the discharge through a Venturimeter as,

$$Q = C \times a_2 \times v_2 \tag{3.4}$$

Where  $C$  = coefficient of Venturimeter

By substituting the values of  $v_2$  of Equation 3.3 in Equation 3.4 and simplifying the equation, we have the discharge through a Venturimeter as,

$$Q = \frac{C \cdot a_1 \cdot a_2}{\sqrt{a_1^2 - a_2^2}} \sqrt{2gh} \tag{3.5}$$

#### IV. RESULTS AND DISCUSSION

This section presents the results and discussion of this work; the performance evaluation of the Venturimeter using Bernoulli's and Continuity equations as stated in section 3 are presented.

##### 4.1 Analysis of the Venturimeter Flow Rig

In this study, the analysis of the discharge of the Venturimeter flow rig was performed with the following data: A Venturimeter with a 25.4mm diameter at inlet and 10mm at the throat is laid with its axis horizontal shown in Figure 3.1. During the flow, the recorded pressure head of the large section is 6.5 millimetres and that at the throat is 4.25 millimetres. Assuming the metre coefficient,  $C$  is 0.99, then:

We know that the area at the inlet,

$$a_1 = \frac{\pi}{4} \times (d_1^2) = \frac{\pi}{4} \times (0.0254^2) = 5.07 \times 10^{-4} \text{ m}^2$$

And the area at throat

$$a_2 = \frac{\pi}{4} \times (d_2^2) = \frac{\pi}{4} \times (0.01^2) = 7.86 \times 10^{-4} \text{ m}^2$$

and the discharge through the Venturimeter is given as Equation 3.5,

$$Q = \frac{C \cdot a_1 \cdot a_2}{\sqrt{a_1^2 - a_2^2}} \sqrt{2gh}$$

Substituting the values in the equation for  $Q$ , we have that, the discharge at the pressure head ( $h$ ) of 0.00225 m is  $Q = 0.52$  litres/s. The excel spreadsheet program was used to compute and analyse the relationship between discharge and head of the flow discharge from the Venturimeter flow rig is presented in Figure 4.1. In the analysis, a fixed value of  $h_2$  was employed while varying the value of  $h_1$  and the difference between  $(h_1 - h_2)$  equals to  $h$  as shown in Table 4.1.

**Table 4.1: Showing differences in heads by varying  $h_1$  and the corresponding discharge**

SN	$h_1$ (mm)	$h_2$ (mm)	$h = h_1 - h_2$ (mm)	h (m)	Discharge q (Litres/sec)
1	5.5	4.25	1.25	0.00125	0.40
2	6.5	4.25	2.25	0.00225	0.52
3	7.5	4.25	3.25	0.00325	0.63
4	8.5	4.25	4.25	0.00425	0.72
5	9.5	4.25	5.25	0.00525	0.80
6	10.5	4.25	6.25	0.00625	0.87

The corresponding values for the discharge  $q$  was recorded and plotted on a graph of discharge  $q$  against  $h$  as shown in Figure 4.1 as scatter plots and Figure 4.2 a 3D plot as a linear relationship between discharge and head.

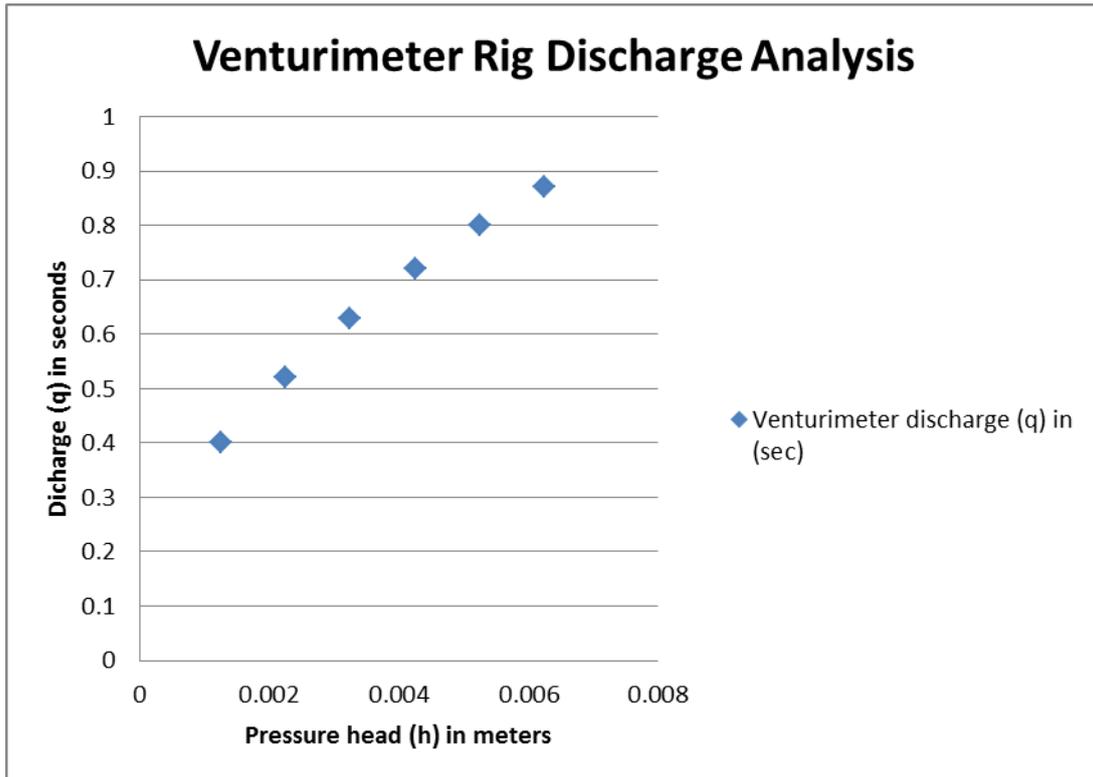


Figure 4.1: Shows the relationship between the pressure head and the discharge.

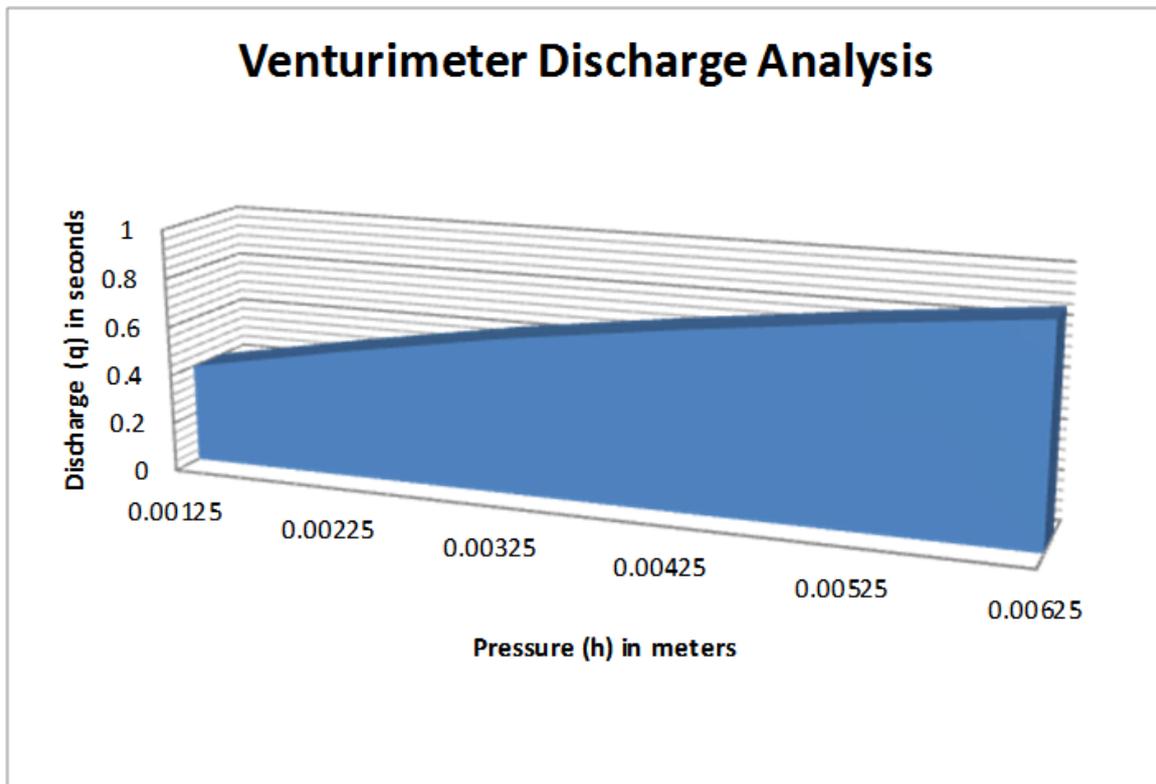


Figure 4.2: Shows a 3D linear relationship between the pressure head and the discharge of the Venturimeter flow rig.

**4.2 Computation Analysis of a Standard Khurmi Venturimeter**

The standard KHURMI (2006) experimental data are as follows: A Venturimeter has an area ratio of 9 to 1, the larger diameter being 300 mm. during the flow, the recorded pressure head in the large section is 6.5 metres and that at the throat is 4.25 metres. Assuming the metre coefficient, C is 0.99, the computed result of the discharge through the Venturimeter is presented as follows:

$$h = h_1 - h_2 = 6.5 - 4.25 = 2.25 \text{ m}$$

where h = difference in pressure head

h<sub>1</sub> = pressure head in the large section

h<sub>2</sub> = pressure head at the throat

Applying the discharge equation which is given in Equation 3.5 as,

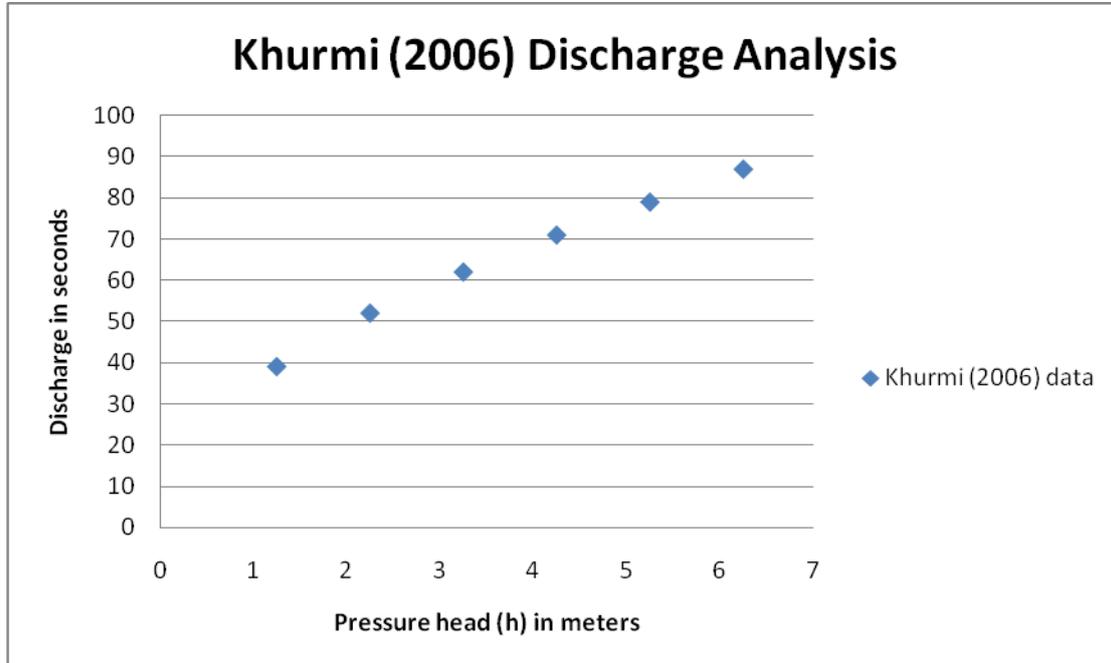
$$Q = \frac{C \cdot a_1 a_2}{\sqrt{a_1^2 - a_2^2}} \sqrt{2gh}$$

The discharge through the metre is equal to **52 litres/s** at the pressure head (h) of 2.25m (see Khurmi, 2006) an excel spreadsheet program was used for the computation.

However, increasing the value of the pressure head produces a corresponding increase in discharge as shown in Table 4.1. And if these values are plotted on a graph, the result is as shown in Figure 4.3 and Figure 4.4 as scatter plots and 3D plot respectively.

**Table 4.2: Showing differences in heads by varying  $h_1$  and the corresponding discharge**

SN	$h_1$ (m)	$h_2$ (m)	$h = h_1 - h_2$ (m)	Discharge q (Litres/sec)
1	5.5	4.25	1.25	39.00
2	6.5	4.25	2.25	52.00
3	7.5	4.25	3.25	62.00
4	8.5	4.25	4.25	71.00
5	9.5	4.25	5.25	79.00
6	10.5	4.25	6.25	87.00



**Figure 4.3: Shows the relationship between the pressure head and the discharge.**

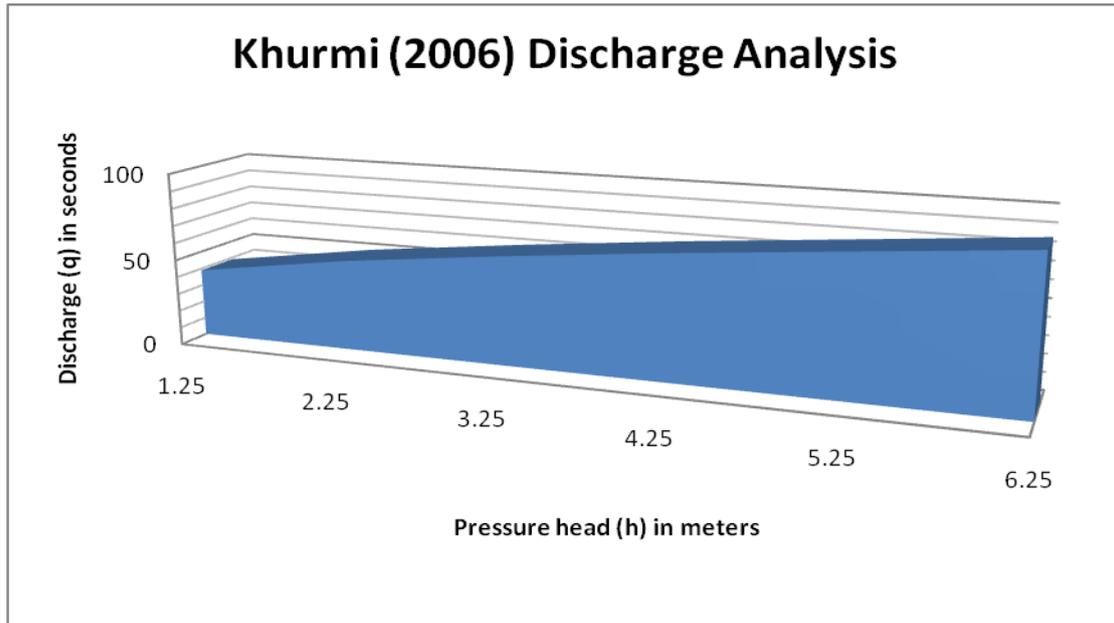


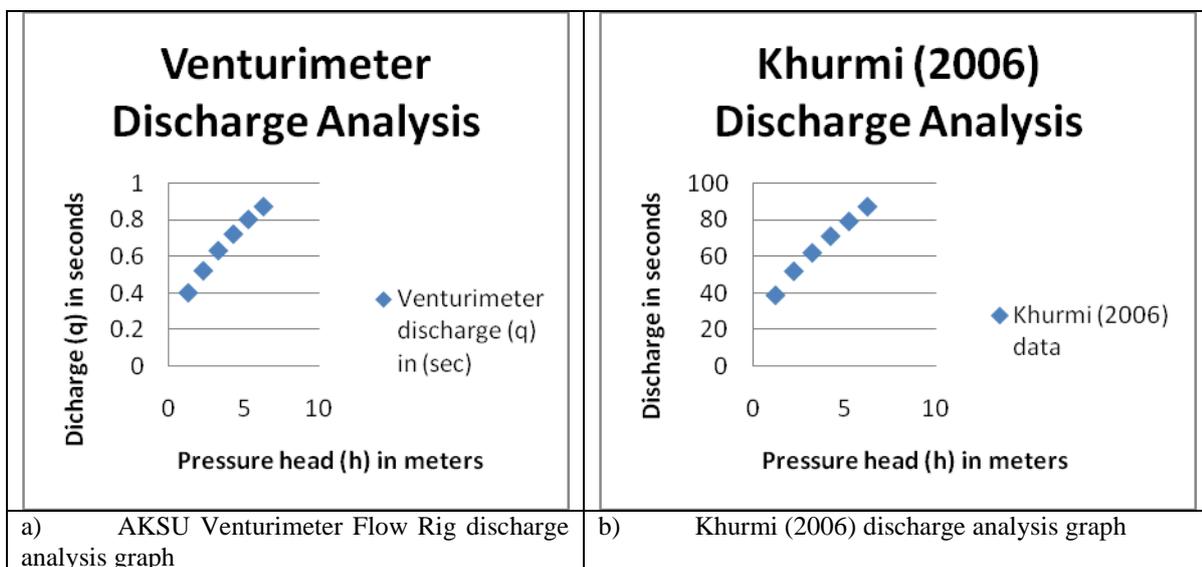
Figure 4.4: Shows a 3D linear relationship between the pressure head and the discharge of the Khurmi Venturimeter.

4.4 VALIDATION AND DISCUSSION OF RESULTS

The results of the Venturimeter flow rig were validated against the standard Khurmi (2006) results and they were in good agreement since the trends were the same. In each case, as the pressure head increases, there was an increase in discharge in both results as shown in Table 4.3. The characteristic curve of both plots is parabolic as shown in Figure 4.5a and Figure 4.5b respectively. This indicated that the higher the head, the higher the flow discharge as presented in Figure 4.5; hence confirming the effectiveness of the Bernoulli's principles and continuity equation in the analysis of flow discharge through Venturimeter.

Table 4.3: Shows the Venturimeter flow rig data against the Khurmi (2006) data

SN	$h = h_1 - h_2$ (m)	Venturimeter rig discharge q (sec)	$h = h_1 - h_2$ (m)	KHURMI discharge q (sec)
1	0.00125	0.40	1.25	39.00
2	0.00225	0.52	2.25	52.00
3	0.00325	0.63	3.25	62.00
4	0.00425	0.72	4.25	71.00
5	0.00525	0.80	5.25	79.00
6	0.00625	0.87	6.25	87.00



a) AKSU Venturimeter Flow Rig discharge analysis graph

b) Khurmi (2006) discharge analysis graph

Figure 4.5: Validation of Venturimeter Flow Rig discharge against Khurmi (2006) discharge analysis

## V. CONCLUSION

The Venturimeter flow rig was designed, constructed and tested. The project was successfully completed and the aims achieved. The results were analysed and compared with a standard Khurmi (2006) analysis of flow discharge through Venturimeter and was in good agreement; hence confirming the usefulness of the Bernoulli's principles and continuity equation in the analysis of flow discharge through Venturimeter. The idea will be effectively applied in the control and measurement of flow along pipeline in oil field, for irrigation purposes, automotive industry, wastewater collection systems and treatment plants. The Venturimeter flow rig manufactured is portable with the capability of easy assembly and disassembly. This flow system is valuable for practical demonstration of fluid measurement and control in Fluid mechanics studies in Mechanical Engineering Laboratory. The cost is affordable due to the use of locally available material; and the cost will further reduce significantly if the Venturimeter flow rig is mass produced.

## ACKNOWLEDGEMENT

I will like to express my gratitude to Asuquo J. Otoy, a Technologist, Department of Mechanical Engineering, Akwa Ibom State University (AKSU), Nigeria and my former student Wilfred Cyrcus Effiong for their contributions during the manufacturing phase of this project.

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